

**AMENDMENTS TO THE CLAIMS**

Please amend claims 17, 23 and 31 as shown below, and cancel claims 22 and 27.

1. (Currently Amended) A solvent extraction mixture for extracting oil from an oil bearing material ~~so as to form an extracted oil comprised of greater than 95% by weight triglycerides and other non-polar constituents, with said solvent having a polarity no greater than about 0 and a viscosity ranging between about 0.3 centipoise and about 2.6 centipoise, whereby the triglycerides are miscible in said solvent at a temperature ranging between about 35° C and about 55° C and after extraction of the triglycerides said solvent and the triglycerides form a miscella, and at a temperature ranging between about 15° C and about 25° C, said miscella will form distinct solvent and oil layers that can be separated, said, the~~ solvent extraction mixture comprising:

oil-bearing material that presents a combination of triglyceride oil and phospholipid oil for extraction; and  
a solvent at a temperature ranging from 35°C to 55°C, the solvent having a viscosity ranging from 0.3 to 2.6 centipoise and a polarity index no greater than about 0, the solvent containing

- B<sup>1</sup>
- (a) ~~an amount of a low molecular weight hydrocarbon constituent having a viscosity of less than 2.6 centipoise; and,~~
- (b) a halocarbon constituent selected from the group consisting of fluorocarbon-solvent or a chlorocarbon-solvent, and chlorofluorocarbon materials in an effective amount to provide selective extraction of the triglyceride oil in preference to the phospholipid oil, as compared to extraction using the hydrocarbon constituent alone—wherein said chlorocarbon is selected from the group consisting of CH<sub>2</sub>Cl<sub>2</sub>, C<sub>2</sub>H<sub>3</sub>Cl<sub>3</sub>, and C<sub>2</sub>HCl<sub>3</sub>, with the provisos that (i) when said fluorocarbon is dichlorotrifluoroethane, said hydrocarbon is not n-pentane or isopentane; (ii) when said fluorocarbon is dichloropenta-fluoropropane, said hydrocarbon is not a C<sub>6</sub>-aliphatic or C<sub>6</sub>-cycloaliphatic hydrocarbon; and (iii) when said fluorocarbon is perfluorohexane, said hydrocarbon is not isohexane.

2. (Currently Amended) The solvent extraction mixture of claim 1 wherein ~~said~~ the hydrocarbon constituent is of ~~the~~ a formula  $C_nH_{(2n+2)}$  or  $C_nH_{2n}$  with n equal to between 5 and 8.

3. (Currently Amended) The solvent extraction mixture of claim 2 wherein ~~said~~ the hydrocarbon constituent is a hexane.

4. (Currently Amended) The solvent extraction mixture of claim 1 wherein ~~said~~ the halocarbon constituent is selected as the fluorocarbon ~~having~~ has a polarity index of less than 0.1.

5. (Currently Amended) The solvent extraction mixture of claim 4 wherein ~~said~~ the fluorocarbon has a polarity index ranging between about - 2.0 and about 0.1 and a dielectric constant ranging between about 1.7 and about 2.0.

6. (Cancelled)

7. (Cancelled)

8. (Cancelled)

9. (Currently Amended) The solvent extraction mixture of claim 3 wherein ~~said~~ the hexane is selected from the group consisting of straight-chained hexanes, branch-chained hexanes, and mixtures thereof.

10. (Currently Amended) The solvent extraction mixture of claim 1 wherein ~~said~~ the halocarbon constituent is selected as the fluorocarbon solvent ~~is~~ further selected from the group consisting of  $C_nH_{(2n+2)-x}F_x$ , where n equals between 4-8 and x equals between 1-17;  $C_nF_{(2n+2)}$ , where n equals between 5-8;  $C_nCl_{(2n+2)-x}F_x$ , where n equals between 1-6 and x equals between 1-13;  $C_nH_{(2n+2)-(x+f)}Cl_xF_f$ , where n equals between 1-4, x equals between 1-9, and f equals between 1-9; and,  $C_nH_{(2n+2)-x}Cl_x$ , where n equals between 1-4, and x equals between 1-9.

11. (Currently Amended) The solvent extraction mixture of claim 10 wherein ~~said~~ the fluorocarbon solvent ~~is~~ selected from the group consisting of  $C_5H_2F_{10}$ ,  $C_6HF_{13}$ ,  $C_7HF_{15}$ ,  $C_{10}HF_{21}$ ,  $C_5F_{12}$ ,  $C_7F_{16}$ ,  $C_6F_{14}$ ,  $C_8F_{18}$ ,  $C_2Cl_3F_3$ ,  $CCl_3F$ ,  $C_3Cl_2F_6$ ,  $C_4Cl_2F_8$ ,  $C_4Cl_3F_7$ ,  $C_6ClF_{13}$ ,  $C_3HCl_2F_5$ , and  $C_2HCl_2F_3$ .

12. (Currently Amended) The solvent extraction mixture of claim 1 wherein the halocarbon constituent is selected as the ~~said~~ fluorocarbon solvent ~~is~~ further selected from the group consisting of hydrofluorocarbon, perfluorocarbon, hydrochlorofluorocarbon, and combinations thereof.

13. (Currently Amended) The solvent extraction mixture of claim 1 wherein the halocarbon constituent is selected as the ~~said~~ fluorocarbon ~~is~~ being a hydrofluorocarbon.

14. (Currently Amended) The solvent extraction mixture of claim 1 wherein the halocarbon constituent is selected as the said fluorocarbon solvent is equal to and the effective amount ranges between 60% and 70% by volume of said the solvent.

15. (Cancelled)

16. (Currently Amended) A solvent extraction mixture for extracting oil from an oil bearing material ~~so as to form an extracted oil comprised of greater than 95% by weight non-polar constituents, with said solvent having a polarity no greater than about 0 and a viscosity less than about 2.6 centipoise, whereby the non-polar constituents are miscible in said solvent at a temperature ranging between about 35°C and about 55°C and after extraction of the non-polar constituents, said solvent and the non-polar constituents separate at a temperature ranging between about 15°C and about 25°C, forming distinct solvent and oil layers that can be separated, said, the solvent~~ extraction mixture comprising:

oil-bearing material that presents a combination of triglyceride oil and phospholipid oil for extraction; and

a solvent at a temperature ranging from 35°C to 55°C, the solvent having a viscosity ranging from 0.3 to 2.6 centipoise and a polarity index no greater than about 0, the solvent containing

(a) ~~an amount of a low molecular weight hydrocarbon constituent having a viscosity of less than 2.6 centipoise; and,~~

(b) a halocarbon constituent in an effective amount to provide selective extraction of the triglyceride oil in preference to the phospholipid oil, as compared to extraction using the hydrocarbon constituent alone

~~(a) an amount of a low molecular weight hydrocarbon; and,~~

~~(b) a non-polar halogenated solvent;~~

~~with the provisos that (i) when said fluorocarbon is~~

~~dichlorotrifluoroethane, said hydrocarbon is not n-pentane or~~

~~isopentane; (ii) when said fluorocarbon is dichloropenta-~~

~~fluoropropane, said hydrocarbon is not a C<sub>6</sub>-aliphatic or C<sub>6</sub>~~

~~cycloaliphatic hydrocarbon; and (iii) when said fluorocarbon is~~

~~perfluorohexane, said hydrocarbon is not isohexane.~~

17-30 (Previously Cancelled)

31. (Previously Added) A solvent for extracting oil from an oil bearing material so as to form an extracted oil comprised of greater than 95% by weight triglycerides and other

non-polar constituents, with said solvent having a polarity no greater than about 0 and a viscosity ranging between about 0.3 centipoise and about 2.6 centipoise, whereby the triglycerides are miscible in said solvent at a temperature ranging between about 35° C and about 55° C and after extraction of the triglycerides said solvent and the triglycerides form a miscella, and at a temperature ranging between about 15° C and about 25° C, said miscella will form distinct solvent and oil layers that can be separated, said solvent comprising:

- (a) an amount of a low molecular weight hydrocarbon having a viscosity of less than 2.6 centipoise; and,
- (b) a fluorocarbon solvent or a chlorocarbon solvent wherein said chlorocarbon is selected from the group consisting of  $\text{CH}_2\text{Cl}_2$ ,  $\text{C}_2\text{H}_3\text{Cl}_3$ , and  $\text{C}_2\text{HCl}_3$ ;

and wherein said fluorocarbon solvent is selected from the group consisting of  $\text{C}_5\text{H}_2\text{F}_{10}$ ,  $\text{C}_6\text{HF}_{13}$ ,  $\text{C}_7\text{HF}_{15}$ ,  $\text{C}_{10}\text{HF}_{21}$ ,  $\text{C}_5\text{F}_{12}$ ,  $\text{C}_7\text{F}_{16}$ ,  $\text{C}_8\text{F}_{18}$ ,  $\text{C}_2\text{Cl}_3\text{F}_3$ ,  $\text{CCl}_3\text{F}$ ,  $\text{C}_3\text{Cl}_2\text{F}_6$ ,  $\text{C}_4\text{Cl}_2\text{F}_8$ ,  $\text{C}_4\text{Cl}_3\text{F}_7$ , and  $\text{C}_6\text{ClF}_{13}$ .

32. (Previously Added) A solvent for extracting oil from an oil bearing material so as to form an extracted oil comprised of greater than 95% by weight non-polar constituents, with said solvent having a polarity no greater than about 0 and a viscosity less than about 2.6 centipoise, whereby the non-polar constituents are miscible in said solvent at a temperature ranging between about 35° C and about 55° C and after extraction of the non-polar constituents, said solvent and the non-polar constituents separate at a temperature ranging between about 15° C and about 25° C, forming distinct solvent and oil layers that can be separated, said solvent comprising:

- (a) an amount of a low molecular weight hydrocarbon; and,
- (b) a non-polar halogenated solvent;

wherein said non-polar-halogenated solvent is selected from the group consisting of  $\text{CH}_2\text{Cl}_2$ ,  $\text{C}_2\text{H}_3\text{Cl}_3$ ,  $\text{C}_2\text{HCl}_3$ ,  $\text{C}_5\text{H}_2\text{F}_{10}$ ,  $\text{C}_6\text{HF}_{13}$ ,  $\text{C}_7\text{HF}_{15}$ ,  $\text{C}_{10}\text{HF}_{21}$ ,  $\text{C}_5\text{F}_{12}$ ,  $\text{C}_7\text{F}_{16}$ ,  $\text{C}_8\text{F}_{18}$ ,  $\text{C}_2\text{Cl}_3\text{F}_3$ ,  $\text{CCl}_3\text{F}$ ,  $\text{C}_3\text{Cl}_2\text{F}_6$ ,  $\text{C}_4\text{Cl}_2\text{F}_8$ ,  $\text{C}_4\text{Cl}_3\text{F}_7$ , and  $\text{C}_6\text{ClF}_{13}$ .